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(54) POROUS HONEYCOMB FILTER AND ITS MANUFACTURING METHOD

(57) Abstract: A porous honeycomb filter having a controlled pore size distribution which comprises a material containing cordierite as a primary crystal phase, characterized in that it has a pore size distribution in which the pore volume of the pores having a pore diameter of loss than 10 μ m is 15% or less of the total pore volume, the pore volume of the pores having a pore diameter of 10 to 50 μ m accounts for 75% or more relative to the total pore volume, and the pore volume of the pores having a pore diameter of more than 50 μ m is 10% or less of the total pore volume. The porous honeycomb filter exhibits improved efficiency for capturing particulate contaminants and the like, and also can prevent the increase of pressure loss due to the clogging of pores thereof, in particular, when used in a diesel engine developed in recent years which adopts high pressure fuel injection, a common rail type device and the like.

SPECIFICATION

TECHNICAL FIELD

This invention pertains to a type of porous honeycomb filter and its manufacturing method. More specifically, this invention pertains to a type of porous honeycomb filter characterized by the fact that it has a high efficiency in trapping fine particles (particulates), etc., can prevent an increase in pressure loss due to the clogging of pores, and, in particular, can display its characteristics for diesel engines that have adopted high-pressure fuel injection, common rail type device, etc., in recent years, as well as a method for manufacturing it.

CONVENTIONAL TECHNOLOGY

In recent years, as a device for removing particulates from exhaust gas, a type of porous honeycomb filter has been adopted. The porous honeycomb filter has a structure in which

multiple through holes that open on the exhaust-gas inlet side end surface and exhaust-gas outlet side end surface have their openings alternately sealed on the two end surfaces, so that the exhaust gas that flows in from the exhaust-gas inlet side end surface is forced to flow through the partition walls between the various through holes (with multiple pores on the walls), and the particulates in the exhaust gas are trapped and removed.

For the porous honeycomb filter, depending on the particle size of the particulates in the exhaust gas, the trapping efficiency, pressure loss, etc., are a function of the size of the pores formed on the wall between the through holes. Consequently, there is a demand for control of the pore size distribution.

In the prior art, porous honeycomb filters are usually made of cordierite or silicon carbide having a high heat resistance. Japanese Kokai Patent Application No. Hei 5[1993]-23512 disclosed a type of porous honeycomb filter, characterized by the fact that it is made of silicon carbide that allows easy control of the pore size, with the average pore size being 1-15 μ m, and the pore size distribution is controlled so that the pore size is distributed over a very narrow range with a standard deviation (SD) of 0.20 or smaller.

On the other hand, Japanese Kokai Patent Application No. Hei 9[1997]-77573 disclosed a type of honeycomb filter with an average pore size of 25-40 μ m, characterized by the fact that it is a honeycomb filter made of cordierite with a controlled pore size; as kaolin and aluminum oxide are not contained as the feed material used to form cordierite, the porosity is increased, and it is manufactured using a method in which the feed material is prepared by adding a certain type of organic foaming agent or combustible substance in a feed material of cordierite containing aluminum hydroxide with a controlled particle size (the proportion of the powder with a particle size of 0.5-3 μ m and the powder with a particle size of 5-15 μ m with respect to the total amount of aluminum hydroxide is 50-100%), fused silica (average particle size of 30-100 μ m), and talc.

However, for the aforementioned honeycomb filter, because the pore size is mainly controlled by aluminum hydroxide, an organic foaming agent, or combustible substance, although the average pore size can be controlled, it is nevertheless impossible to have the pore size distribution within the desired narrow range. Also, because aluminum hydroxide is used in the form of fine particles, the thermal expansion coefficient becomes higher, and this is undesired.

In order to solve this problem, Japanese Patent Nos. 2578176 and 2726616 described a manufacturing method of a honeycomb filter, characterized by the fact that it makes use of a feed material prepared by adding graphite as a pore forming agent into a feed material used to form cordierite in the form of a mixture of various components such as talc, silica, alumina, and kaolin as powders having prescribed particle sizes and in prescribed proportions; the pore size distribution has the following features: [1] the proportion of pores with a size of 2 μ m or smaller

among all of the pores is 7 vol% or less, [2] the proportion of pores with a size of 100 μm or larger among all of the pores is 10 vol% or less.

However, for such honeycomb filters, because no special consideration is given to the fact that the various components are different from each other with respect to ease in controlling the pore size, the ability to control the lower limit or upper limit of the pore size distribution is insufficient, and it is impossible to have a pore size distribution within a prescribed narrow range.

In order to solve this problem, Japanese Kokoku Patent No. Hei 7[1995]-38930 described a manufacturing method of a honeycomb filter, characterized by the fact that in consideration of the fact that the various components talc, silica, alumina, and kaolin are different from each other with respect to ease in controlling the pore size, the feed material used to form cordierite is prepared by adjusting the two components talc and silica such that the proportion of the powder with a particle size of 150 µm or larger among the entire feed material is 3 wt% or less, and the proportion of the particles with particle size of 45 µm is 25 wt% or less; the obtained honeycomb filter has a proportion of pores with a size of 10-50 µm, among all of the pores, of 52.0-74.1 vol%.

For such a honeycomb filter, for the first time, the pore size has been controlled to within a range as narrow as 10-50 µm. Compared with the aforementioned various types of honeycomb filters made of cordierite, the trapping efficiency is higher, and it is also better in preventing an increase in the pressure loss due to clogging. Also, because the particle size of talc is smaller, it is possible to realize a lower thermal expansion coefficient.

However, in recent years, because of improvements in the diesel engine (by adopting high-pressure fuel injection, common rail device, etc.), the exhaust rate has been reduced, and the particulates have become smaller and more uniform (the particle size of the particulates is usually about $1 \mu m$). Consequently, there is a high demand for the development of a type of honeycomb filter with its pore size being under high degree of control.

On the other hand, because the aforementioned honeycomb filter is manufactured without knowing that kaolin, in the feed material used to form cordierite, is closely associated with the formation of pores of 10 µm or smaller, it is impossible to form pores with a size of 10-50 µm at a high proportion of 75.0 vol% or higher. Consequently, it cannot meet the aforementioned demand requested in recent years.

The purpose of this invention is to solve the aforementioned problems of the conventional methods by providing a type of porous honeycomb filter and its manufacturing method, characterized by the fact that it has a high efficiency in trapping fine particles (particulates), etc., can prevent an increase in pressure loss due to clogging of the pores, and, in

particular, can display the characteristics to meet the demand related to the diesel engines that have adopted high-pressure fuel injection, common rail device, etc., in recent years.

DISCLOSURE OF THE INVENTION

In order to solve the aforementioned problems, the present inventors have performed extensive research. As a result of this research work, it was found that by controlling the particle size of the silica component in the feed material used to form cordierite, and, at the same time, lowering the concentration of kaolin, it is possible to control the pore size distribution in the desired range. As a result, this invention was reached.

That is, this invention provides a type of porous honeycomb filter characterized by the following facts: the porous honeycomb filter is made of a material with cordierite having a controlled pore size distribution as its primary crystal phase; its pore size distribution has the following features: the volume of pores with a size of $10 \, \mu m$ or smaller is 15% or less of the total pore volume; the volume of pores with a size of $10\text{-}50 \, \mu m$ is 75% or more of the total pore volume; and the volume of pores with a size of $50 \, \mu m$ or larger is 10% or less of the total pore volume.

For the honeycomb filter of this invention, the porosity of the honeycomb filter is preferably 50-75%, more preferably 65-75%, or most preferably 68-75%. Also, the thermal expansion coefficient of the honeycomb filter at a temperature of 40-80°C is preferably 1.0×10^{-6} °C or lower.

Also, this invention provides a method for manufacturing a porous honeycomb filter characterized by the fact that in the manufacturing method of a porous honeycomb filter using a ceramic feed material used to form cordierite as the principal feed material, the feed material used to form cordierite contains 10 wt% or less of kaolin, and, for the silica (SiO₂) source component other than kaolin and talc, the particle size distribution is such that the proportion of the powder with a particle size of 75 μ m or larger is 1 wt% or less.

The manufacturing method of a honeycomb filter in this invention differs from the manufacturing method described in Japanese Kokai Patent Application No. Hei 9[1997]-77573 in that the proportion of kaolin is 1-10 wt%.

It is preferred that the silica (SiO_2) source component other than kaolin and talc contain at least one type of quartz or fused silica.

It is preferred that the feed material used to form cordierite contain at least one type of aluminum oxide and aluminum hydroxide as the alumina (Al_2O_3) source component. In this case, for the alumina (Al_2O_3) source component, it is preferred that it contain 15-45 wt% of aluminum hydroxide with a particle size of 1-10 μ m, or 0-20 wt% of aluminum oxide with a particle size of 4-8 μ m.

Also, it is preferred that the feed material used to form cordierite contain 37-40 wt% of talc as the magnesia (MgO) source component. In this case, it is preferred that the particle size of talc is 5-40 µm.

As the ceramic feed material, it is preferred that it contain 1-4 parts by weight of a foaming resin with respect to 100 parts by weight of the feed material used to form cordierite.

OPTIMUM FORM FOR EMBODIMENT OF THE INVENTION

In the following, the form for embodiment of this invention will be explained in detail.

1. Porous honeycomb filter

The porous honeycomb filter of this invention is a porous honeycomb filter containing cordierite with its pore size distribution being highly controlled to a prescribed range as the primary crystal phase.

In the following, a detailed discussion will be presented.

The porous honeycomb filter of this invention has cordierite as its primary crystal phase. The cordierite may be the orientated, non-orientated, α crystalline, β crystalline form, etc.

Also, it may contain mullite, zircon, aluminum titanate, clay-bound silicon carbide, zirconia, spinel, indialite, sapphirine, corundum, titania, and other crystal phases.

These crystal phases may be used either alone or as a mixture of several types.

The pore size distribution of the porous honeycomb filter of this invention has the following features: the volume of pores with a size of 10 μ m or smaller is 15% or less of the total pore volume; the volume of pores with a size of 10-50 μ m is 75-100% of the total pore volume; and the volume of pores with a size of 50 μ m or larger is 10% or less of the total pore volume.

If the volume of pores with a size of 10-50 µm is less than 75% of the total pore volume, the volume of pores with a size of 10 µm or smaller becomes over 15% of the total pore volume, the pressure loss due to clogging of the pores rises, and, when a catalyst is applied on the filter, —the pressure loss due to clogging of pores with the catalyst rises. On the other hand, if the volume of pores with a size of 10-50 µm is 75% or less of the total pore volume, and the volume of pores with a size of 50 µm or larger is 10% or more of the total pore volume, the trapping efficiency of the particulates decreases.

In particular, in recent years, with improvements in the diesel engines, the particles have become smaller and more uniform. Consequently, if the volume of pores with a size of 10-50 μ m is not 75% or more of the total pore volume, the efficiency is not high, and it is hard to improve the trapping efficiency of the particulates corresponding to said improvement of diesel engines.

For the honeycomb filter of this invention, in order to reduce the pressure loss and to increase the trapping efficiency, the porosity is preferably 50-75%, more preferably 65-75%, or

most preferably 68-75%. Also, in order to improve the resistance to heat impact for use at high temperatures, the thermal expansion coefficient at temperature of $40-800^{\circ}$ C is preferably 1.0×10^{-6} C or lower.

The honeycomb filter in this invention has a structure in which multiple through holes that open on the exhaust-gas inlet side end surface and exhaust-gas outlet side end surface are alternately sealed on the two end surfaces. However, there is no specific limitation on the shape of the honeycomb filter. For example, it may be a cylinder with a circular or elliptic shape of the end surfaces, or a polygon with a triangular, square, or other polygonal shape of the end surfaces, or a cylinder or polygon with the side surface bent to a < shape, etc. Also, there is no special limitation on the shape of the through holes. For example, the cross sections of the through holes may have a square, octagonal, or other polygonal shape, circular shape, elliptic shape, etc.

The porous honeycomb filter of this invention can be manufactured using the following method.

2. Method for manufacturing porous honeycomb filter

In the method for manufacturing a porous honeycomb filter of this invention, the porous honeycomb filter is manufactured from a ceramic feed containing a material used to form cordierite as its principal feed material; in this method, the components in the feed material used to form cordierite and particle sizes are controlled within certain ranges.

In the following, the method will be discussed in more detail.

For the feed material used to form cordierite in this invention, the silica (SiO_2) source component other than kaolin and talc has a particle size distribution such that the proportion of the powder with a particle size of 75 μ m or larger is 1 wt% or less, preferably 0.5 wt% or less.

As a result, pores with a size in a narrow range of $10-50~\mu m$ can be formed at a very high rate, and the manufactured honeycomb filter has a high trapping efficiency and is free of an increase in the pressure loss due to clogging of pores.

That is, it has been found that in this invention, the silica (SiO_2) source component other than kaolin and talc in the feed material used to form cordierite differs from the other components in that pores with a size nearly equal to the particle size of the component can be formed, and that by crushing the large particle powder with a particle size of 75 μ m or larger, because they contribute little to the formation of pores with a size of 10 μ m or less, it is possible to form pores with a size in the narrow range of 10-50 μ m at a very high rate.

Examples of the silica (SiO₂) source component other than kaolin and talc include quartz, fused silica, mullite, etc. Among them, it is preferred that at least quartz or fused silica be contained because they have high stability up to a high temperature during sintering and they allow easy control of the pore size.

It is preferred that 15-20 wt% of said silica (SiO₂) source component be contained in the feed material used to form cordierite. Also, although it may contain Na₂O, K₂O, and other impurities, it is preferred that the total content of these impurities in the silica (SiO₂) source component be 0.01 wt% or less so as to prevent an increase in the thermal expansion coefficient.

The feed material used to form cordierite used in this invention may also contain 10 wt% or less of kaolin.

If the content of kaolin is over 10 wt%, it is impossible to suppress the formation of pores with a size of 10 μ m or smaller, and it thus becomes impossible to have the volume of pores with a size of 10-50 μ m to be 75% or more of the total pore volume even when the particle size of the silica (SiO₂) source component other than kaolin and talc is controlled.

That is, according to this invention, in addition to said control of the particle size distribution of said silica (SiO₂) source component, in consideration of the fact that kaolin in the feed material used to form cordierite is related to the formation of pores with a size of 10 μ m or smaller, it has been found that by having the content of kaolin to be 10 wt% or less, it is possible to almost completely suppress the formation of pores with a size of 10 μ m or smaller.

Also, according to this invention, from the viewpoint of control of the pore size distribution, the content of kaolin is suppressed. In order to realize this, the method of this invention differs from the manufacturing method described in Japanese Kokai Patent Application No. Hei 9[1997]-77573 in that the content [of kaolin] is 1-10 wt%.

Although kaolin may contain mica, quartz, etc., as impurities, in order to prevent an increase in the thermal expansion coefficient, it is preferred that the content of these impurities be 2 wt% or less.

In order to have the various components of the feed material used to form cordierite having a theoretical composition of cordierite crystals, in addition to said silica (SiO₂) source component and kaolin, it is necessary to add other components, such as talc or some other magnesia (MgO) component, aluminum oxide, aluminum hydroxide, and other alumina (Al₂O₃) -source components, etc.

In consideration of the fact that less impurities are contained, as the alumina (Al₂O₃) source component, it is preferred that aluminum oxide and/or aluminum hydroxide be contained. Aluminum hydroxide is particularly preferred.

As far as the particle size of the alumina (Al_2O_3) source component is concerned, in order to enable a reduction of the thermal expansion coefficient and in performing high-precision control of the pore size distribution by controlling the particle size distribution of said silica (SiO_2) source component, when aluminum hydroxide is used, the particle size is preferably 1-10 μ m; when aluminum oxide is used, the particle size is preferably 4-8 μ m.

Also, for the alumina (Al_2O_3) source component, it is preferred that 15-45 wt% of aluminum hydroxide be contained in the feed material used to form cordierite, or that 0-20 wt% of aluminum oxide be contained in it.

As the magnesia (MgO) source component, for example, talc, magnesite, etc., may be used. Among them, talc is preferred. It is preferred that 37-40 wt% of talc be contained in the feed material used to form cordierite. In order to lower the thermal expansion coefficient, the particle size of talc is preferably 5-40 μ m, or more preferably 10-30 μ m.

Talc or some other magnesia (MgO) source component used in this invention may contain Fe₂O₃, CaO, Na₂O, K₂O, etc., as impurities.

The content of Fe_2O_3 in the magnesia (MgO) source component is preferably 0.1-2.5 wt%. When this range is observed, it is possible to lower the thermal expansion coefficient, and at the same time to obtain a high porosity.

In order to lower the thermal expansion coefficient, the total content of CaO, Na_2O , and K_2O in the magnesia (MgO) source component is preferably 0.35 wt% or less.

According to the manufacturing method in this invention, when the porosity is further increased, it is possible to further increase the trapping efficiency and to reduce the pressure loss. In consideration of this fact, it is preferred that the feed material used to form cordierite also contain pore forming agent, etc., as additives.

Examples of pore forming agents include acrylic microcapsules and other foaming resins, graphite, wheat flour, starch, phenolic resin, polymethyl methacrylate, polyethylene, polyethylene terephthalate, etc. Among them, acrylic microcapsules and other foaming resins are preferred.

For acrylic microcapsules, and other foaming resins, because they are hollow [particles], even a small amount can form a honeycomb filter with a high porosity, and heating of the pore forming material in the sintering step of the operation can be suppressed. Consequently, even when the pore forming agent is added to form a honeycomb filter with a high porosity, the heat generated in the sintering step is small, and the generation of thermal stress can be alleviated.

When a larger amount of foaming resin is added, while the obtained honeycomb filter has a very high porosity, the strength decreases, and it is prone to damage in canning. Consequently, the amount [of the foaming resin] with respect to 100 parts by weight of the feed material used to form cordierite is preferably 1.0-4.0 parts by weight, or more preferably 1.5-3.0 parts by weight.

According to this invention, as needed, other additives such as a binder and dispersant for accelerating dispersion in the medium liquid may be contained.

Examples of binders that may be added include hydroxypropylmethylcellulose, methylcellulose, hydroxyethylcellulose, carboxymethylcellulose, polyvinyl alcohol, etc.

Examples of the dispersants that may be used include ethylene glycol, dextrin, fatty acid soap, polyalcohol, etc.

As needed, the aforementioned additives may be used either alone or as a mixture of several types.

There is no special limitation on [the feed material used to form cordierite used in this invention], except that the contents and particle size of the prescribed components in the feed material used to form cordierite should be controlled to within certain ranges. For example, it is possible to manufacture the honeycomb filter in the following manufacturing process.

First of all, 3-5 parts by weight of a binder, 2-40 parts by weight of a pore forming agent, 0.5-2 parts by weight of a dispersant, and 10-40 parts by weight of water are loaded in 100 parts by weight of said feed material used to form cordierite, then the mixture is blended to form a plastic.

Molding of the plastic feed material is performed using any of the following methods: extrusion molding method, injection molding method, press molding method, method in which through holes are formed after the ceramic feed material is molded into a cylindrical shape, and other methods. Among these methods, the extrusion molding method is preferred because it allows continuous molding easily, and it can orientate the cordierite crystals to realize a low thermal expansion property.

The feed molding is dried by hot air, microwave drying, dielectric drying, drying under a reduced pressure, vacuum drying, freeze drying, etc. Among them, the hot-air drying method, microwave drying method, or their combination with dielectric drying are preferred because they allow fast drying of the entire molding uniformly.

Finally, sintering of the dry molding is performed corresponding to the size of the dry molding. Usually, sintering is preferably carried out at a temperature of 1410-1440°C for 3-7 h. Also, it is possible to perform the drying step and sintering step continuously.

In the following, this invention will be explained in detail with reference to application examples. However, this invention is not limited to these application examples.

1. Evaluation methods

For the honeycomb filter samples prepared in the application examples and comparative examples to be explained later, an evaluation was performed using the following methods.

(1) Pore size distribution, average size of pores

The pore size distribution and average pore size were measured using a mercury press-in type porosimeter manufactured by the Micromeritex Co. [transliteration]

(2) Porosity

With the true specific gravity of cordierite taken as 2.52 g/cc, from the total pore volume, the porosity was calculated.

(3) Trapping efficiency

The exhaust gas containing soot and produced from a soot generator was fed through the honeycomb filter prepared in each application example or comparative example for a prescribed time (2 min). The soot contained in the exhaust after passing through the filter was trapped with filter paper, then the weight of the soot (W¹) was measured. Also, the soot in the exhaust gas that did not pass through said filter was also trapped with filter paper, and the weight of the soot (W²) was also measured. From the obtained weights (W¹) and (W²), the trapping efficiency was calculated using the following equation (1).

$$(W^2-W^1)/(W^2) \times 100$$
 (1)

(4) Pressure loss due to trapping of soot

For each of the honeycomb filters prepared in the application examples and comparative examples, the following test was performed. A ring with an internal diameter Φ of 130 mm was pressed in contact with each of the two end surfaces. Via said rings, the soot produced in a soot generator was fed to flow to within 130 mm Φ of the honeycomb filter, and 10 g of the soot were trapped.

With soot trapped on the honeycomb filter, air was fed to flow at a rate of 2.27 Nm³/min, then the difference in pressure before and after the filter was measured to evaluate the pressure loss in the state with trapped soot.

2. Application Examples, Comparative Examples

-APPLICATION EXAMPLE 1

Components with the average particle size and particle size distribution listed in Table 1, including talc (average particle size of 20 μ m and proportion of powder of particles with a particle size of 75 μ m or larger of 4 wt%), fused silica B (average particle size of 35 μ m and proportion of powder with a particle size of 75 μ m or larger of 0.5 wt%), and aluminum hydroxide (average particle size of 2 μ m and proportion of powder with a particle size of 75 μ m or larger of 0 wt%) were mixed with the additives listed in Table 2, that is, with proportion of 37 wt% of talc, 19 wt% of fused silica B, and 44 wt% of aluminum hydroxide, to form a feed material used to form cordierite.

As listed in Table 2, in 100 parts by weight of the prepared feed material used to form cordierite, 20 parts by weight of graphite, 7 parts by weight of polyethylene terephthalate, 7 parts by weight of polymethyl methacrylate, 4 parts by weight of hydroxypropylmethylcellulose, 0.5 part by weight of potassium laurate soap, and 30 parts by weight of water were added, then the mixture was blended to form a plastic feed material. The obtained plastic feed material was molded into a cylindrical shape using a vacuum clay blender, followed by molding into a honeycomb shape in an extrusion molding machine.

The obtained molding was subjected to dielectric drying, then bone dried with hot air. Its two end surfaces were then cut out with prescribed dimensions.

The through holes on the dry honeycomb body were then alternately sealed on the two end surfaces by means of a slurry prepared from a cordierite with the same composition as aforementioned.

Finally, it was sintered at 1420°C for 4 h, forming a honeycomb filter with a size of 144 mm Φ x 152 mm L [length], wall thickness of 300 μ m, and cell number of 300 cells/inch².

APPLICATION EXAMPLE 2

A honeycomb filter was prepared in the same way as in Application Example 1, except that instead of fused silica B (average particle size of 35 μ m and proportion of powder with a particle size of 75 μ m or larger of 0.5 wt%) used in Application Example 1, quartz B (average particle size of 19 μ m and proportion of powder with a particle size of 75 μ m or larger of 0.3 wt%) was added.

COMPARATIVE EXAMPLE 1

A honeycomb filter was prepared in the same way as in Application Example 1, except that instead of fused silica B (average particle size of 35 µm and proportion of powder with a particle size of 75 µm or larger of 0.5 wt%) used in Application Example 1, fused silica A —(average particle size of 40 µm and proportion of powder with a particle size of 75 µm or larger of 6 wt%) was added.

APPLICATION EXAMPLE 3

Just as in Application Example 1, components with the average particle size and particle size distribution listed in Table 1, that is, talc (average particle size of 20 µm and proportion of powder of particles with a particle size of 75 µm or larger of 4 wt%), kaolin (average particle size of 10 µm and proportion of powder with a particle size of 75 µm or larger of 2 wt%), quartz D (average particle size of 5 µm and proportion of powder with a particle size of 75 µm or larger of 0.1 wt%), aluminum oxide (average particle size of 6 µm and proportion of powder with a

particle size of 75 µm of 0.2 wt%), and aluminum hydroxide (average particle size of 2 µm and proportion of powder with a particle size of 75 µm or larger of 0 wt%), were mixed as listed in Table 2, that is, of 40 wt% of talc, 1 wt% of Kaolin, 21 wt% of quartz D, 19 wt% of aluminum oxide, and 19 wt% of aluminum hydroxide were mixed to prepare a feed material used to form cordierite. In 100 parts by weight of the obtained feed material used to form cordierite, as a pore forming agent, 20 parts by weight of graphite, 10 parts by weight of polyethylene terephthalate, and 10 parts by weight of polymethyl methacrylate were added. Otherwise, the operation was performed in the same way as in Application Example 1 to form a honeycomb filter.

APPLICATION EXAMPLE 4

Just as in Application Example 1, components with the average particle size and particle size distribution listed in Table 1, that is, talc (average particle size of 20 µm and proportion of powder of particles with a particle size of 75 µm or larger of 4 wt%), kaolin (average particle size of 10 µm and proportion of powder with a particle size of 75 µm or larger of 2 wt%), quartz B (average particle size of 19 µm and proportion of powder with a particle size of 75 µm or larger of 0.3 wt%), aluminum oxide (average particle size of 6 µm and proportion of powder with a particle size of 75 µm of 0.2 wt%), and aluminum hydroxide (average particle size of 2 µm and proportion of powder with a particle size of 75 µm or larger of 0 wt%), were mixed as listed in Table 2, that is, 40 wt% of talc, 3 wt% of kaolin, 20 wt% of quartz B, 18 wt% of aluminum oxide, and 19 wt% of aluminum hydroxide were mixed to prepare a feed material used to form cordierite. In 100 parts by weight of the obtained feed material used to form cordierite, as a pore forming agent, 20 parts by weight of graphite, 9 parts by weight of polyethylene terephthalate, and 9 parts by weight of polymethyl methacrylate were added. Otherwise, the operation was performed in the same way as in Application Example 1 to form a honeycomb filter.

-APPLICATION EXAMPLE 5

Just as in Application Example 4, as listed in Table 2, instead of quartz B listed in Table 1 (average particle size of 19 μ m and proportion of powder with a particle size of 75 μ m or larger of 0.3 wt%), quartz D (average particle size of 5 μ m and proportion of powder with a particle size of 75 μ m or larger of 0.1 wt%) was mixed; also, for 100 parts by weight of the obtained feed material used to form cordierite, as a pore forming agent, 25 parts by weight of graphite, 5 parts by weight of polyethylene terephthalate, and 10 parts by weight of polymethyl methacrylate were added. Otherwise, the operation was performed in the same way as in Application Example 4 to form a honeycomb filter.

APPLICATION EXAMPLE 6

Just as in Application Example 4, as listed in Table 2, instead of quartz B listed in Table 1 (average particle size of 19 µm and proportion of powder with a particle size of 75 µm or larger of 0.3 wt%), quartz E (average particle size of 10 µm and proportion of powder with a particle size of 75 µm or larger of 0.1 wt%) was mixed; also, for 100 parts by weight of the obtained feed material used to form cordierite, as a pore forming agent, 20 parts by weight of graphite and 4 parts by weight of polyethylene terephthalate were added. Otherwise, the operation was performed in the same way as in Application Example 4 to form a honeycomb filter.

APPLICATION EXAMPLE 7

Just as in Application Example 4, as listed in Table 2, instead of quartz B listed in Table 1 (average particle size of 19 µm, proportion of powder with a particle size of 75 µm or larger of 0.3 wt%), fused silica B (average particle size of 35 µm, proportion of powder with a particle size of 75 µm or larger of 0.5 wt%) was mixed, and, for 100 parts by weight of the obtained feed material used to form cordierite, as a pore forming agent, 20 parts by weight of graphite, 3 parts by weight of polyethylene terephthalate, and 9 parts by weight of polymethyl methacrylate were added. Otherwise, the operation was performed in the same way as in Application Example 4 to form a honeycomb filter.

APPLICATION EXAMPLE 8

Just as in Application Example 4, as listed in Table 2, instead of quartz B listed in Table 1 (average particle size of 19 µm, proportion of powder with a particle size of 75 µm or larger of 0.3 wt%), fused silica C (average particle size of 16 µm, proportion of powder with a particle size of 75 µm or larger of 1 wt%) was mixed, and, for 100 parts by weight of the obtained feed material used to form cordierite, as a pore forming agent, 10 parts by weight of graphite and 17 parts by weight of polymethyl methacrylate were added. Otherwise, the operation was performed in the same way as in Application Example 4 to form a honeycomb filter.

COMPARATIVE EXAMPLE 2

Just as in Application Example 4, as listed in Table 2, instead of quartz B listed in Table 1 (average particle size of 19 μ m, proportion of powder with a particle size of 75 μ m or larger of 0.3 wt%), quartz A (average particle size of 20 μ m, proportion of powder with a particle size of 75 μ m or larger of 8 wt%) was mixed, and, for 100 parts by weight of the obtained feed material used to form cordierite, as a pore forming agent, 20 parts by weight of

graphite, 7 parts by weight of polyethylene terephthalate, and 9 parts by weight of polymethyl methacrylate were added. Otherwise, the operation was performed in the same way as in Application Example 4 to form a honeycomb filter.

COMPARATIVE EXAMPLE 3

Just as in Application Example 4, as listed in Table 2, instead of quartz B listed in Table 1 (average particle size of 19 μ m, proportion of powder with a particle size of 75 μ m or larger of 0.3 wt%), quartz C (average particle size of 5 μ m, proportion of powder with a particle size of 75 μ m or larger of 3 wt%) was mixed, and, for 100 parts by weight of the obtained feed material used to form cordierite, as a pore forming agent, 20 parts by weight of graphite, 10 parts by weight of polyethylene terephthalate, and 10 parts by weight of polymethyl methacrylate were added. Otherwise, the operation was performed in the same way as in Application Example 4 to form a honeycomb filter.

COMPARATIVE EXAMPLE 4

Just as in Application Example 4, as listed in Table 2, instead of quartz B listed in Table 1 (average particle size of 19 μ m, proportion of powder with a particle size of 75 μ m or larger of 0.3 wt%), fused silica D (average particle size of 70 μ m, proportion of powder with a particle size of 75 μ m or larger of 39 wt%) was mixed, and, for 100 parts by weight of the obtained feed material used to form cordierite, as a pore forming agent, 20 parts by weight of graphite, 6 parts by weight of polyethylene terephthalate, and 7 parts by weight of polymethyl methacrylate were added. Otherwise, the operation was performed in the same way as in Application Example 4 to form a honeycomb filter.

APPLICATION EXAMPLE 9

Just as in Application Example 4, as listed in Table 2, 40 wt% of talc, 5 wt% of kaolin, —19 wt% of quartz B, 17 wt% of aluminum oxide, and 19 wt% of aluminum hydroxide were mixed to prepare a feed material used to form cordierite. For 100 parts by weight of the obtained feed material used to form cordierite, as a pore forming agent, 20 parts by weight of graphite, 7 parts by weight of polyethylene terephthalate, and 7 parts by weight of polymethyl methacrylate were added. Otherwise, the operation was performed in the same way as in Application Example 4 to form a honeycomb filter.

APPLICATION EXAMPLE 10

Just as in Application Example 4, as listed in Table 2, 40 wt% of talc, 10 wt% of kaolin, 17 wt% of quartz B, 16 wt% of aluminum oxide, and 17 wt% of aluminum hydroxide were

mixed to prepare a feed material used to form cordierite. For 100 parts by weight of the obtained feed material used to form cordierite, as a pore forming agent, 10 parts by weight of graphite, 8 parts by weight of polyethylene terephthalate, and 15 parts by weight of polymethyl methacrylate were added. Otherwise, the operation was performed in the same way as in Application Example 4 to form a honeycomb filter.

COMPARATIVE EXAMPLE 5

Just as in Application Example 4, as listed in Table 2, 40 wt% of talc, 15 wt% of kaolin, 14 wt% of quartz B, 15 wt% of aluminum oxide, and 16 wt% of aluminum hydroxide were mixed to prepare a feed material used to form cordierite. For 100 parts by weight of the obtained feed material used to form cordierite, as a pore forming agent, 20 parts by weight of graphite, 4 parts by weight of polyethylene terephthalate, and 9 parts by weight of polymethyl methacrylate were added. Otherwise, the operation was performed in the same way as in Application Example 4 to form a honeycomb filter.

COMPARATIVE EXAMPLE 6

Just as in Application Example 4, as listed in Table 2, 40 wt% of talc, 19 wt% of kaolin, 12 wt% of quartz B, 14 wt% of aluminum oxide, and 15 wt% of aluminum hydroxide were mixed to prepare a feed material used to form cordierite. For 100 parts by weight of the obtained feed material used to form cordierite, as a pore forming agent, 20 parts by weight of graphite, 4 parts by weight of polyethylene terephthalate, and 7 parts by weight of polymethyl methacrylate were added. Otherwise, the operation was performed in the same way as in Application Example 4 to form a honeycomb filter.

APPLICATION EXAMPLE 11

Just as in Application Example 10, as listed in Table 2, a feed material used to form
-cordierite was prepared without adding graphite, polyethylene terephthalate, and polymethyl
methacrylate as a pore forming agent, and a honeycomb filter was prepared in the same way as in
Application Example 10 except that 2.4 parts by weight of acrylic microcapsules (commercial
name: F-50E, product of Matsumoto Oils & Fats Pharmaceutical Co., Ltd.) were added to
100 parts by weight of the feed material used to form cordierite.

APPLICATION EXAMPLE 12

Just as in Application Example 10, as listed in Table 2, 40 wt% of talc, 0 wt% of kaolin, 21 wt% of quartz D, 16 wt% of aluminum oxide, and 23 wt% of aluminum hydroxide were mixed to prepare a feed material used to form cordierite. For 100 parts by weight of the obtained

feed material used to form cordierite, as a pore forming agent, 10 parts by weight of graphite, 5 parts by weight of polyethylene terephthalate, and 5 parts by weight of polymethyl methacrylate were added and, as a foaming resin, 1.8 parts by weight of acrylic microcapsules were added. Otherwise, the operation was performed in the same way as in Application Example 10 to form a honeycomb filter.

APPLICATION EXAMPLE 13

Just as in Application Example 10, as listed in Table 2, 40 wt% of talc, 5 wt% of kaolin, 19 wt% of quartz B, 17 wt% of aluminum oxide, and 19 wt% of aluminum hydroxide were mixed to prepare a feed material used to form cordierite. For 100 parts by weight of the obtained feed material used to form cordierite, as a pore forming agent, 20 parts by weight of graphite were added and, as a foaming resin, 2.8 parts by weight of acrylic microcapsules were added. Otherwise, the operation was performed in the same way as in Application Example 10 to form a honeycomb filter.

3. Discussion

In Application Examples 1-13, a silica source component other than kaolin and talc has a particle size distribution with a proportion of powder with a particle size of 75 µm or larger of 1.0 wt% or less was added. In these application examples, honeycomb filters with the particle size of 50 µm controlled at 10% or less of the overall pore volume were obtained. For these obtained honeycomb filters, it is possible to realize a trapping efficiency as high as 85% or higher. In particular, in Application Examples 3 and 5, in which the silica source component other than kaolin and talc has a particle size distribution such that the proportion of powder with a particle size of 75 µm or larger is 0.1 wt% or less, it is possible to obtain honeycomb filters with the proportion of the pores with a size of 50 µm or larger controlled at 2% or less of the overall pore volume. For the obtained honeycomb filters, it is possible to realize a trapping

•efficiency as high as 94% or higher.

On the other hand, in Comparative Examples 1-4, the particle size distribution of the silica source component other than kaolin and talc is such that the proportion of powder with a particle size of 75 μ m or larger is 1.0 wt% or larger. In these comparative examples, honeycomb filters with a proportion of the volume of pores having a size of 50 μ m or larger of 10% or more than the overall pore volume were obtained. For the obtained honeycomb filters, the trapping efficiency is as low as 75% or lower.

In Application Examples 1-13, in which the content of kaolin is 10 wt% or less, it is possible to obtain honeycomb filters for which the proportion of the volume of pores with a size of $10~\mu m$ or smaller is controlled at 15% or smaller than the overall pore volume. It is estimated

that when a catalyst is applied on the filter, clogging of pores by the catalyst can be suppressed, and the pressure loss in the trapping of soot is low.

On the other hand, in Comparative Examples 5 and 6, in which the content of kaolin is over 10 wt%, for the obtained honeycomb filters, the proportion of the volume of pores with a size of 10 µm or smaller is over 15% of the overall pore volume. It is estimated that when a catalyst is applied on the filter, the pressure loss due to clogging of pores with the catalyst is high.

In Application Examples 11-13, in which 1.8-2.8 parts by weight of a foaming agent are added with respect to 100 parts by weight of the feed material used to form cordierite, it is possible to obtain honeycomb filters with a porosity of 68-75%. For the obtained honeycomb filters, it is possible to realize a trapping efficiency as high as 91% or higher. Also, the pressure loss is 8.5 KPa or lower, and the pressure loss in the soot trapped state is low.

Also, in Application Example 12, in which a honeycomb filter is prepared by adding 3.2 parts by weight of the foaming agent, the obtained honeycomb filter has a porosity of 80%, yet the structural strength may be insufficient.

Table 1. Components

| Components of feed material used to form cordierite | Average particle size (µm) | Proportion of powder with particle size of 75 µm or larger (wt%) |
|-----------------------------------------------------|----------------------------|------------------------------------------------------------------|
| Talc | 20 | 4 |
| Quartz | 10 | 2 |
| Fused silica A | 20 | 8 |
| Fused silica B | 19 | 0.3 |
| Fused silica C | 5 | 3 |
| Fused silica D | 5 | 0.1 |
| Fused silica E | 10 | 0.1 |
| Aluminum oxide A | 40 | 6 |
| Aluminum oxide B | 35 | 0.5 |
| Aluminum oxide C | 16 | 1 |
| Aluminum oxide D | 70 | 39 |
| Aluminum oxide | 6 | 0.2 |
| Aluminum hydroxide | 2 | 0 |

Table 2. Composition of feed material (wt%).

| | | | Table 4. | Composition | 2001 | | | | | |
|------------------------|-------|--------|----------------------------------------|----------------|-----------|-----------|-----------|------------|--------------------|---------------|
| | | LL. | Feed materials used to form cordierite | sed to form co | ordierite | | | Pore tor | Pore forming agent | |
| | | | | tuononmo | Aliminim | Aluminum | Granhite | PET "1 | PMM *2 | Foaming resin |
| | F | Voolin | Silica source component | Malibalia | | | Smith 1 | ind other) | in other | *4 (narte hy |
| OZ | aic | Nacien | | Content | oxide | hydroxide | (parts by | (pairs by | (pairs by | o (paris by |
| | (wt%) | (wt%) | Component | (wt%) | (wt%) | (wt%) | weight) | weight) | weight) | weight) |
| Application Example 1 | 37 | 0 | Fused silica | 19 | 0 | 44 | 50 | 7 | 7 | 0 |
| | 5 | | Suprt. B | 40 | C | 44 | 20 | 7 | 7 | 0 |
| Application Example 2 | ره/ | | Grank | 2 2 | ę | 9 | 20 | 10 | 10 | 0 |
| Application Example 3 | 9 | - | Quartz D | 17 | 100 | 2 0 | 200 | 6 | 6 | 0 |
| Application Example 4 | \$ | 3 | Quartz B | 2 2 | 9 | 2 0 | 22 | Ľ | Ç | 0 |
| Application Example 5 | 40 | က | Quartz D | 22 | 0] | 5 | 3 8 | , | 2 | c |
| Application Example 6 | 40 | က | Quartz E | 20 | 18 | 19 | 25 | 4 | | > |
| Application Example 7 | 40 | ဧ | Fused silica B | 8 | 18 | 19 | 20 | 3 | o | 0 |
| Application Example 8 | 40 | က | Fused silica | 70 | 18 | 19 | 9 | 0 | 17 | 0 |
| | 4 | u | Oliarty B | ē | 17 | 19 | 20 | 2 | 2 | 0 |
| Application Example 9 | 2 5 | 2 5 | Quarty B | 1 | 16 | 17 | 10 | 8 | 15 | 0 |
| Application Example 10 | 3 5 | 2 9 | Quartz B | + | 2 9 | 17 | 0 | 0 | 0 | 2.4 |
| Application Example 11 | € 4 | 2 | Cuaric D | 3 | 9 | 33 | 9 | 5 | 2 | 1.8 |
| Application Example 12 | € : |) · | Cualiz D | 5 | 100 | 9 | 2 | C | 0 | 2.8 |
| Application Example 13 | 40 | 2 | Quartz B | 2 | | 2 | 3 | , | | |
| Comparative Example 1 | 37 | 0 | Fused silica A | 19 | 0 | 44 | 50 | 7 | 7 | 0 |
| Comparative Evample 2 | Q# | 63 | Quartz A | ଛ | 18 | 19 | 20 | 7 | 6 | 0 |
| Comparative Example 3 | 8 | 8 | Quartz C | 20 | 48 | 19 | 8 | 우 | 9 | 0 |
| Comparative Example 4 | 40 | က | Fused silica D | 20 | 18 | 19 | 50 | 9 | 7 | 0 |
| Comparative Example 5 | 40 | 15 | Quartz B | 14 | 15 | 16 | 8 | 4 | 6 | 0 |
| Comparative Example 6 | Ş | 9 | Ouartz B | 12 | 14 | 15 | 20 | 4 | 7 | 0 |
| Comparative Example o | } | 2 | | | | | | | | |

*1 PET: Polyethylene terephthalate
*2 PMM: Polymethyl methacrylate
*3 Foaming resin: Acrylic microcapsules

Table 3. Properties

| | | | | | | , | | | | | | | | | | | | | | | |
|------------------------|-------------|-------------------|-----------------------|-----------------------|-----------------------|-----------------------|-----------------------|-----------------------|-----------------------|-----------------------|-----------------------|------------------------|------------------------|------------------------|------------------------|-----------------------|-----------------------|-----------------------|-----------------------|-----------------------|-----------------------|
| Transing | efficiency | (%) | 98 | 88 | 94 | 87 | 92 | 93 | 87 | 85 | 68 | 06 | 91 | 98 | 96 | 71 | 89 | 75 | 48 | 6 | 88 |
| Pressure | loss due to | trapping (KPa) | 9.4 | 8.9 | 8.7 | 9.0 | 8.5 | 10.4 | 6.6 | 10.2 | 9.1 | 9.2 | 8.5 | 7.8 | 7.4 | 9.4 | 9.1 | 8.7 | 10.1 | 9.7 | 10.2 |
| Thermal | expansion | (x 10-6/°C) | 9.0 | 2.0 | 9.0 | 2.0 | 9.0 | 9.0 | 9.0 | 9.0 | 2.0 | 0.7 | 6.0 | 6.0 | 1.0 | 9:0 | 2.0 | 9.0 | 2.0 | 0.7 | 0.7 |
| Average | pore | size (µm) | 56 | 22 | 17 | 21 | 16 | 19 | 23 | 20 | 20 | 19 | 21 | . 18 | 25 | 28 | 22 | 17 | 33 | 19 | 17 |
| Pore size distribution | i C | - mm oc | 6 | 2 | 7 | 2 | 2 | 3 | 8 | 10 | 9 | 5 | 10 | 9 | 10 | 15 | 17 | 12 | 88 | 9 | 7 |
| | 0 | 10-50 µm | 88 | 91 | 93 | 88 | 88 | 90 | 85 | 22 | 98 | 80 | 75 | 82 | 82 | 83 | 79 | 77 | 57 | 75 | 70 |
| | 1 | -10 µm | 2 | 2 | 2 | 5 | 10 | 7 | 7 | 13 | 8 | 15 | 15 | 12 | 8 | 2 | 4 | 11 | 5 | 19 | 24 |
| | Porosity | (%) | 09 | 62 | 99 | 63 | 65 | 54 | 58 | 55 | 61 | 26 | 89 | 72 | 75 | 99 | 62 | 65 | 22 | 58 | 26 |
| | No. | | Application Example 1 | Application Example 2 | Application Example 3 | Application Example 4 | Application Example 5 | Application Example 6 | Application Example 7 | Application Example 8 | Application Example 9 | Application Example 10 | Application Example 11 | Application Example 12 | Application Example 13 | Comparative Example 1 | Comparative Example 2 | Comparative Example 3 | Comparative Example 4 | Comparative Example 5 | Comparative Example 6 |

INDUSTRIAL APPLICATION FIELD

As explained in the above, according to the porous honeycomb filter and its manufacturing method of this invention, the trapping efficiency of particulates is high, and it is possible to prevent an increase in the pressure loss due to clogging of the pores. In particular, this invention provides a type of porous honeycomb filter that can display characteristics appropriate for diesel engines that have adopted high-pressure fuel injection, common rail device, etc., and developed in recent years, along with its manufacturing method.

CLAIMS

1. A type of porous honeycomb filter characterized by the following facts:

the porous honeycomb filter is made of a material with cordierite, having a controlled pore size distribution, as its primary crystal phase;

its pore size distribution has the following features: the volume of pores with a size of $10~\mu m$ or smaller is 15% or less of the total pore volume; the volume of pores with a size of 10- $50~\mu m$ is 75% or more of the total pore volume; and the volume of pores with a size of $50~\mu m$ or larger is 10% or less of the total pore volume.

- 2. The porous honeycomb filter described in Claim 1, characterized by the fact that the porosity of the honeycomb filter is 50-75%.
- 3. The porous honeycomb filter described in Claim 2, characterized by the fact that the porosity of the honeycomb filter is 65-75%.
- 4. The porous honeycomb filter described in any of Claims 1-3, characterized by the fact that the thermal expansion coefficient of the honeycomb filter at a temperature of $40-800^{\circ}$ C is 1.0×10^{-6} /°C or lower.
- 5. A method for manufacturing a porous honeycomb filter characterized by the following facts: in the manufacturing method of a porous honeycomb filter with a ceramic feed material used to form cordierite being the principal feed material:

the feed material used to form cordierite contains 0-10 wt% or less [sic; 0-10%] of kaolin, and, for the silica (SiO₂) source component other than kaolin and talc, the particle size distribution is such that the proportion of the powder with a particle size of 75 μ m or larger is 1 wt% or less.

6. The manufacturing method of a porous honeycomb filter described in Claim 5, characterized by the fact that said feed material used to form cordierite contains 1-10 wt% of kaolin.

- 7. The manufacturing method of a porous honeycomb filter described in Claim 5 or 6, characterized by the fact that the silica (SiO₂) source component other than kaolin and talc contains at least one type of quartz or fused silica.
- 8. The manufacturing method of a porous honeycomb filter described in any of Claims 5-7, characterized by the fact that said feed material used to form cordierite contains at least one type of aluminum oxide and aluminum hydroxide as the alumina (Al₂O₃) source component.
- 9. The manufacturing method of a porous honeycomb filter described in Claim 8, characterized by the fact that for as said alumina (Al_2O_3) source component, 15-45 wt% of aluminum hydroxide with a particle size of 1-10 μ m is contained.
- 10. The manufacturing method of a porous honeycomb filter described in Claim 8 or 9, characterized by the fact that for said alumina (Al_2O_3) source component, 0-20 wt% of aluminum hydroxide with a particle size of 4-8 μ m is contained.
- 11. The manufacturing method of a porous honeycomb filter described in any of Claims 5-10, characterized by the fact that for said magnesia (MgO) source component, 37-40 wt% of talc is contained.
- 12. The manufacturing method of a porous honeycomb filter described in Claim 11, characterized by the fact that the particle size of talc is $5-40 \mu m$.
- 13. The manufacturing method of a porous honeycomb filter of Claims 5-12, characterized by the fact that said ceramic feed material contains 1-4 parts by weight of a foaming resin with respect to 100 parts by weight of the feed material used to form cordierite.

INTERNATIONAL SEARCH REPORT

International application No.
PCT/JP01/08720

| A CLASSIFICATION OF SUBJECT MATTER | | | | | | | | | |
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| C. DOCU | MENTS CONSIDERED TO BE RELEVANT | | | | | | | | |
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| Special categories of cited documents: "A" document defining the general state of the art which is not considered to be of particular relevance carlier documents but published on or after the international filling date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention date: "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified) "O" document referring to an oral disclosure, use, exhibition or other means "F" document published prior to the international filing date but later than the priority date claimed "I" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention document of particular relevance; the olaimed invention cannot be considered to involve an invention at particular relevance; the olaimed invention cannot be considered to involve an invention of the particular relevance; the olaimed invention cannot be considered to involve an invention of the particular relevance; the olaimed invention cannot be considered to involve an invention of the particular relevance; the olaimed invention cannot be considered to involve an invention of the particular relevance; the olaimed invention cannot be considered to involve an invention of the particular relevance; the olaimed invention cannot be considered to involve an invention of the particular relevance; the olaimed invention cannot be considered to involve an invention of the particular relevance; the olaimed invention of the priority date and not in conflict with the application of the understand the principle or theory underlying the invention of the priority date and not in conflict with the application of the understand the principle or theory underlying the invention of the priority date after the international filling date or pr | | | | | | | | | |
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/続葉有]

- (54) Title: POROUS HONEYCOMB FILTER AND METHOD FOR MANUFACTURE THEREOF
- (54) 発明の名称: 多孔質ハニカムフィルター及びその製造方法・

(57) Abstract: A porous honeycomb filter having a controlled pore size distribution which comprises a material containing cordierite as a primary crystal phase, characterized in that it has a pore size distribution in which the pore volume of the pores having a pore diameter of less than 10 μ m is 15 % or less of the total pore volume, the pore volume of the pores having a pore diameter of 10 to 50 μ m accounts for 75 % or more relative to the total pore volume, and the pore volume of the pores having a pore diameter of nore than 50 μ m is 10 % or less of the total pore volume. The porous honeycomb filter exhibits improved efficiency for capturing particulate contaminants and the like, and also can prevent the increase of pressure loss due to the clogging of pores thereof, in particular, when used in a diesel engine developed in recent years which adopts high pressure fuel injection, a common rail type device and the like.

(57) 要約:

細孔分布を制御したコーディライトを主結晶相とする材料からなる多孔質ハニカムフィルターである。細孔分布を、細孔径 10μ m未満の細孔容積:全細孔容積の15%以下、細孔径 $10\sim50\mu$ mの細孔容積:全細孔容積の75%以上、細孔径 50μ mを超える細孔容積:全細孔容積の10%以下、とする。この多孔質ハニカムフィルターは、微粒子(パティキュレート)等の捕集効率が高く、かつ細孔の目詰まりによる圧力損失の増大を防止することができ、特に、近年の高圧燃料噴射、コモンレール等を採用したディーゼルエンジンに対応してこれらの特性を発揮することができる。

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1

明 細 書

多孔質ハニカムフィルター及びその製造方法

技術分野

本発明は、多孔質ハニカムフィルター及びその製造方法に関する。さらに詳しくは、微粒子 (パティキュレート) 等の捕集効率が高く、かつ細孔の目詰まりによる圧力損失の増大を防止することができ、特に、近年の高圧燃料噴射、コモンレール等を採用したディーゼルエンジンに対応してこれらの特性を発揮することができる多孔質ハニカムフィルター及びその製造方法に関する。

背景技術

近年、排ガス中の微粒子を除去する装置として、排ガス流入側端面と排ガス排出側端面に開口する複数の貫通孔を、両端面で互い違いに目封じした構造を有し、排ガス流入側端面から流入した排ガスを、強制的に各貫通孔間の隔壁(複数の細孔を有する)を通過させ、排ガス中の微粒子を捕集、除去する多孔質ハニカムフィルターが用いられている。

この多孔質ハニカムフィルターでは、排ガス中の微粒子の粒径との関係で、各質通孔間の隔壁に形成される細孔の孔径をどの程度とするかにより捕集効率、圧力損失等の性能が異なってくる為、細孔分布を制御することが要求されている。

従来、多孔質ハニカムフィルターとしては、耐熱性に優れるコーディエライト製工は炭化ケイ素製のものが多く用いられており、細孔径の制御が容易である炭化ケイ素製の多孔質ハニカムフィルターについては、細孔径の平均値が $1\sim15$ μ mで、細孔分布が標準偏差(SD) 0.20以下と極めて狭い範囲で細孔径を制御したものが開示されている(特開平5-23512号公報)。

他方、細孔の孔径を制御したコーディエライト製のハニカムフィルターとしては、カオリンと酸化アルミニウムをコーディエライト化原料に含有させないことにより気孔率を向上させるとともに、粒径を特定範囲で制御した水酸化アルミニ

ウム(粒径が $0.5\sim3~\mu$ mの粉末と粒径が $5\sim1~5~\mu$ mの粉末とが水酸化アルミニウム全体の $5~0\sim1~0~0$ %を占める)と、溶融シリカ(平均粒径が $3~0\sim1~0~0~\mu$ m)と、タルクからなるコーディライト化原料に、所定の有機発泡剤又は可燃性物質を添加した原料を用いる製造方法により得られた、平均孔径が $2~5\sim4~0~\mu$ mのハニカムフィルターが開示されている(特開平9~-7~7~5~7~3号公報)。

しかし、このハニカムフィルターでは、細孔径を主に水酸化アルミニウムと、 有機発泡剤又は可燃性物質により制御する為、平均細孔径は制御できても細孔分 布を所望の狭い範囲とすることは不可能であった。また、水酸化アルミニウムを 粗粒化する為、熱膨張係数が増大するという問題も有していた。

これに対して、タルク、シリカ、アルミナ、カオリンの各成分を特定の粒径の粉末とし、特定の含有率で混合したコーディライト化原料に、造孔剤としてグラファイトを添加した原料を用いる製造方法により得られた、細孔分布が、それぞれ①細孔径2μm以下の細孔が全細孔中7容積%以下、②細孔径100μm以上の細孔が全細孔中10容積%以下、のハニカムフィルターが開示されている(特許第2578176号公報、特許第2726616号公報)。

しかし、これらのハニカムフィルターでは、各成分毎に細孔径を制御する容易性が異なる点について特に考慮されていない為、細孔分布の下限又は上限を制御するのが限界であり、細孔分布を所望の狭い範囲とすることは不可能であった。

これらに対して、タルク、シリカ、アルミナ、カオリンの各成分毎に細孔径を制御する容易性が異なる点に着目して、タルクとシリカの両成分について、粒径 150μ m以上の粉末を原料全体で3質量%以下とし、かつ粒径 45μ m以下の粉末を25質量%以下に調整したコーディライト化原料を用いる製造方法により得られた、細孔径 $10\sim50\mu$ mの細孔が全細孔中 $52.0\sim74.1$ 容積%を占めるハニカムフィルターが提案されている(特公平7-38930号公報)。

このハニカムフィルターは、細孔径を10~50μmの狭い範囲に制御することをコーディライト製のハニカムフィルターで初めて達成するものであり、前述 した種々のコーディライト製ハニカムフィルターに比べ、捕集効率を向上するこ とができるとともに、目詰まりの防止により圧力損失の増大を防止することができるものである。また、タルクの粒径を小さくすることで、熱膨張係数を小さくすることができるものである。

しかし、近年、排ガス中の微粒子は、ディーゼルエンジンの改良(高圧燃料噴射、コモンレール等が採用されている。)により、排出量の低減化とともに微粒子が小径化、均一化している(微粒子の粒径は、殆ど、略1 μmである。) ことから、細孔径を極めて高度に制御したハニカムフィルターが強く要望されている

これに対して、このハニカムフィルターでは、コーディライト化原料におけるカオリンが 10μ m以下の細孔の形成に深く関与することについて全く意図せずに製造されていたことから、細孔径 $10\sim50\mu$ mの細孔を75.0容積%以上の高率で形成することができず、このような近年の要望に応じることができるものではなかった。

本発明は、上述の問題に鑑みなされたもので、微粒子 (パティキュレート)等の捕集効率が高く、かつ細孔の目詰まりによる圧力損失の増大を防止することができ、特に、近年の高圧燃料噴射、コモンレール等を採用したディーゼルエンジンに対応してこれらの特性を発揮することができる多孔質ハニカムフィルター及びその製造方法を提供することを目的とする。

発明の開示

本発明者は、上述の課題を解決するべく鋭意研究した結果、コーディライト化原料のシリカ成分の粒径を制御するとともに、カオリンを低濃度化することにより、細孔径分布を所望の範囲で高度に制御できることを知見し、本発明を完成させた。

即ち、本発明によれば、細孔分布を制御したコーディライトを主結晶相とする 材料からなる多孔質ハニカムフィルターであって、細孔分布が、細孔径 $10\mu m$ 未満の細孔容積:全細孔容積の15%以下、細孔径 $10\sim50\mu m$ の細孔容積: 全細孔容積の75%以上、細孔径 $50\mu m$ を超える細孔容積:全細孔容積の10 %以下であることを特徴とする多孔質ハニカムフィルターが提供される。

本発明のハニカムフィルターにおいては、ハニカムフィルターの気孔率が、5 $0 \sim 75\%$ であることが好ましく、 $65 \sim 75\%$ であることがより好ましく、 $68 \sim 75\%$ であることが特に好ましい。また、ハニカムフィルターの $40 \sim 80$ 0℃における熱膨張係数が、 1.0×10^{-6} /℃以下であることが好ましい。

また、本発明によれば、コーディエライト化原料を主原料とするセラミックス原料を用いる多孔質ハニカムフィルターの製造方法であって、コーディエライト化原料が、カオリンを、10質量%以下で含有し、かつカオリン及びタルク以外のシリカ(SiO_2)源成分を、粒径 75μ m以上の粉末が1質量%以下で含有する粒径分布としたことを特徴とする多孔質ハニカムフィルターの製造方法が提供される。

本発明のハニカムフィルターの製造方法においては、特開平9-77573号 公報に記載の製造方法と異なり、カオリンを、1~10質量%の割合で含有させ ることができる。

また、カオリン及びタルク以外のシリカ (SiO₂)源成分は、石英、又は溶融シリカの少なくとも一種を含有したものが好ましい。

また、コーディエライト化原料は、アルミナ($A1_2O_3$)源成分として、酸化アルミニウム、又は水酸化アルミニウムの少なくとも一種を含有したものが好ましい。この際、アルミナ($A1_2O_3$)源成分として、粒 $E1\sim10~\mu$ mの水酸化アルミニウムを $15\sim45$ 質量%含有するか、粒 $E4\sim8~\mu$ mの酸化アルミニウムを $0\sim20$ 質量%含有することが好ましい。

また、コーディエライト化原料は、マグネシア(MgO)源成分として、タルクを37~40質量%含有することが好ましく、この際、タルクの粒径は、5~40 μ mであることが好ましい。

また、セラミックス原料として、コーディエライト化原料100重量部に対して、発泡樹脂を1~4重量部含有させたものを用いることも好ましい。

発明を実施するための最良の形態

以下、本発明の実施の形態を、具体的に説明する。

1. 多孔質ハニカムフィルター

本発明の多孔質ハニカムフィルターは、細孔分布を特定の範囲に高度に制御したコーディライトを主結晶相とする多孔質ハニカムフィルターである。

以下、具体的に説明する。

本発明の多孔質ハニカムフィルターは、コーディエライトを主結晶とするものであるが、コーディエライトは、配向、無配向、 α 結晶質、 β 結晶質等のいずれでもよい。

また、ムライト、ジルコン、チタン酸アルミニウム、クレーポンド炭化ケイ素、ジルコニア、スピネル、インディアライト、サフィリン、コランダム、チタニア等の他の結晶相を含有するものであってもよい。

尚、これら結晶相は、1種単独又は2種以上を同時に含有するものであっても よい。

本発明の多孔質ハニカムフィルターにおける細孔分布は、細孔径 10μ m未満の細孔容積が全細孔容積の15%以下、細孔径 $10\sim50\mu$ mの細孔容積が全細孔容積の $75\sim100\%$ 、細孔径 50μ mを超える細孔容積が全細孔容積の10%以下である。

細孔径 $10\sim50\,\mu$ mの細孔容積が全細孔容積の75%未満となって、細孔径 $10\,\mu$ m未満の細孔容積が全細孔容積の15%を超えると、細孔の目詰まりにより圧力損失の増大を生じてしまい、また、フィルターに触媒を付ける場合に、触媒による細孔の目詰まりによって圧力損失の増大を生じてしまう。一方、細孔径 $10\sim50\,\mu$ mの細孔容積が全細孔容積の75%未満となって、細孔径 $50\,\mu$ m を超える細孔容積が全細孔容積の10%を超えると、パティキュレートの捕集効率が低下してしまう。

特に、近年のディーゼルエンジンの改良に伴いパティキュレートが径小化、均一化していることから、細孔径 $10\sim50\mu m$ の細孔容積が全細孔容積の 75% 以上と高効率化しなければ、このようなディーゼルエンジンの改良に対応してパティキュレートの捕集効率を向上させることが困難になる。

本発明のハニカムフィルターは、圧力損失の低減化及び捕集効率の向上という点から、気孔率が $50\sim75\%$ であることが好ましく、気孔率が $65\sim75\%$ であることがより好ましく、気孔率が $68\sim75\%$ であることが特に好ましい。また、高温使用時における耐熱衝撃性の向上という点から、 $40\sim800\%$ における熱膨張係数が 1.0×10^{-6} /%以下であることが好ましい。

本発明のハニカムフィルターは、通常、排ガス流入側端面と排ガス排出側端面に開口する複数の貫通孔を、両端面で互い違いに目封じした構造を有するものであるが、ハニカムフィルターの形状について特に制限はなく、例えば、端面の形状が真円又は楕円の円柱、端面の形状が三角、四角等の多角形である角柱、これらの円柱、角柱の側面がくの字に湾曲した形状等いずれでもよい。また、貫通孔の形状についても特に制限はなく、例えば、断面形状が四角、八角等の多角形、真円、楕円等いずれでもよい。

尚、本発明の多孔質ハニカムフィルターは、次に述べる方法等で製造することができる。

2. 多孔質ハニカムフィルターの製造方法

本発明の多孔質ハニカムフィルターの製造方法は、コーディエライト化原料を 主原料とするセラミックス原料を用いる多孔質ハニカムフィルターを製造する方 法であって、コーディエライト化原料中の特定成分の含有率及び粒径を特定の範 囲に制御するものである。

以下、具体的に説明する。

本発明に用いられるコーディエライト化原料は、カオリン及びタルク以外のシリカ(SiO_2)源成分を、粒径 $75\mu m$ 以上の粉末が1質量%以下、好ましくは 0.5質量%以下の粒径分布としたものである。

これにより、細孔径10~50μmの狭い範囲の細孔を極めて高率で形成することができ、捕集効率が高く、かつ細孔の目詰まりによる圧力損失の増大のないハニカムフィルターを製造することができる。

即ち、本発明は、コーディエライト化原料中のカオリン及びタルク以外のシリカ(SiO。)源成分が、他の成分と異なり、成分粒径に略対応した細孔径の細

孔を形成することができること、及び細孔径 10μ m以下の細孔の形成に殆ど関与しないことに着目し、粒径 75μ m以上の粗粒粉末をカットすることにより、細孔径 $10\sim50\mu$ mの狭い範囲の細孔を極めて高率で形成できることを見出したものである。

カオリン及びタルク以外のシリカ (SiO₂) 源成分としては、石英、溶融シリカ、ムライト等を挙げることができるが、中でも、焼成時に高温まで安定して存在し、細孔径の制御が容易である点で、石英、溶融シリカの少なくとも一種を含有するものが好ましい。

このシリカ (SiO₂) 源成分は、コーディエライト化原料中、 $15\sim20$ 質量%含有させるのが好ましい。また、不純物として Na_2O 、 K_2O 等を含有してもよいが、これら不純物の含有率は、熱膨張係数の増大を防止することができる点で、シリカ (SiO₂) 源成分中、合計で0.01質量%以下であることが好ましい。

本発明で用いられるコーディエライト化原料は、更に、カオリンを10質量% 以下の含有率とするものである。

カオリンが10質量%を超えて含有すると、細孔径 10μ m未満の細孔の形成を抑制できない為、前述したカオリン及びタルク以外のシリカ(SiO_2)源成分の粒径を制御しても細孔径 $10\sim50\mu$ mの細孔容積を全細孔容積の75%以上とすることが不可能となる。

即ち、本発明は、前述したシリカ(SiO_2)源成分の粒度分布の制御に加え、コーディエライト化原料中のカオリンが、主に細孔径 $10\mu m$ 未満の細孔の形成に関与していることに着目し、カオリンの含有率を10質量%以下の低率とすることにより、細孔径 $10\mu m$ 未満の細孔の形成を殆ど抑制できることを見出したものである。

尚、本発明は、細孔分布の制御という点からカオリンの含有率を抑制する為、 特開平9-77573号公報に記載の製造方法と異なり、1~10質量%の範囲 で含有させてもよい。

また、カオリンは、不純物として雲母、石英等を含有してもよいが、これら不

純物の含有率は、熱膨張係数の増大を防止することができる点、2質量%以下であることが好ましい。

本発明に用いられるコーディエライト化原料は、コーディエライト結晶の理論 組成となるように各成分を配合する為、上述したシリカ(SiO_2)源成分及び カオリン以外に、例えば、タルク等のマグネシア(MgO)源成分、酸化アルミ ニウム、水酸化アルミニウム等のアルミナ(Al_2O_3)源成分等を配合する必要 がある。

アルミナ(A 1 2O3)源成分としては、不純物が少ないという点で酸化アルミニウム、又は水酸化アルミニウムのいずれか一種又はこれら両方を含有するものが好ましく、中でも水酸化アルミニウムを含有するものが好ましい。

また、アルミナ($A1_2O_3$)源原料の粒径は、熱膨張係数を低くくすることができるとともに、前述したシリカ(SiO_2)源成分の粒径分布による孔径分布の制御を精密に行うことができる点で、水酸化アルミニウムの場合は $1\sim10~\mu$ mが好ましく、酸化アルミニウムの場合は $4\sim8~\mu$ mが好ましい。

また、アルミナ($A1_2O_3$)源原料は、コーディエライト化原料中、水酸化アルミニウムは $15\sim45$ 質量%含有させることが好ましく、酸化アルミニウムは $0\sim20$ 質量%含有させることが好ましい。

マグネシア(MgO)源成分としては、例えば、タルク、マグネサイト等を挙げることができ、中でも、タルクが好ましい。タルクは、コーディエライト化原料中37~40質量%含有させることが好ましく、タルクの粒径は、熱膨張係数を低くする点から5~40 μ mが好ましく、10~30 μ mがより好ましい。

また、本発明に用いるタルク等のマグネシア(MgO)源成分は、不純物として Fe_2O_3 、CaO、 Na_2O 、 K_2O 等を含有してもよい。

但し、Fe₂O₃の含有率は、マグネシア(MgO)源成分中、0.1~2.5 質量%とするのが好ましい。この範囲の含有率であれば、熱膨張係数を低くくすることができるとともに、高い気孔率を得ることができる。

また、CaO、Na,O、K,Oの含有率は、熱膨張係数を低くするという点から、マグネシア(MgO)源成分中、これら合計で0.35質量%以下とするこ

とが好ましい。

本発明の製造方法では、更に気孔率を増大させることにより、捕集効率を向上させ、かつ圧力損失を低減することができる点で、コーディエライト化原料に、添加剤として、気孔を形成する為の造孔剤等を含有させることが好ましい。

造孔剤としては、例えば、アクリル系マイクロカプセル等の発泡樹脂、グラファイト、小麦粉、澱粉、フェノール樹脂、ポリメタクリル酸メチル、ポリエチレン、又はポリエチレンテレフタレート等を挙げることができるが、中でも、アクリル系マイクロカプセル等の発泡済みの発泡樹脂が好ましい。

アクリル系マイクロカプセル等の発泡済みの発泡樹脂は、中空であることから 少量で高気孔率のハニカムフィルターを得ることができ、焼成工程での造孔材の 発熱を抑える事ができるため、造孔材を添加して高気孔率のハニカムフィルター とする場合でも、焼成工程での発熱が少なく、熱応力の発生を低減することがで きる。

もっとも、発泡樹脂を多量に添加すると、得られるハニカムフィルターの気孔 率が極めて大きくなる反面、強度が低下して、キャニング等の際に、損傷し易く なるので、コーディエライト化原料100重量部に対して、1.0~4.0重量 部含有させることが好ましく、1.5~3.0重量部含有させることがより好ま しい。

本発明においては、必要に応じて、この他の添加剤を含有させることができ、 例えば、バインダー、媒液への分散を促進するための分散剤等を含有させてもよ い。

また、バインダーとしては、例えば、ヒドロキシプロピルメチルセルロース、メチルセルロース、ヒドロキシエチルセルロース、カルボキシルメチルセルロース、ポリビニルアルコール等を挙げることができ、分散剤としては、例えば、エチレングリコール、デキストリン、脂肪酸石鹸、ポリアルコール等を挙げることができる。

なお、以上述べた各添加剤は、目的に応じて1種単独又は2種以上組み合わせ て用いることができる。 本発明においては、コーディエライト化原料中の特定成分の含有率及び粒径を 特定の範囲に制御すること以外について特に制限はなく、例えば、以下に示す製 造工程でハニカムフィルターを製造することができる。

まず、上述したコーディエライト化原料100重量部に対して、バインダー3~5重量部、造孔剤2~40重量部、分散剤0.5~2重量部、水10~40重量部を投入後、混練し、可塑性とする。

次いで、可塑性原料の成形は、押出し成形法、射出成形法、プレス成形法、セラミックス原料を円柱状に成形後貫通孔を形成する方法等で行うことができ、中でも、連続成形が容易であるとともに、コーディエライト結晶を配向させて低熱 膨張性にできる点で押出し成形法で行うことが好ましい。

次いで、生成形体の乾燥は、熱風乾燥、マイクロ波乾燥、誘電乾燥、減圧乾燥、真空乾燥、凍結乾燥等で行うことができ、中でも、全体を迅速かつ均一に乾燥することができる点で、熱風乾燥とマイクロ波乾燥又は誘電乾燥とを組み合わせた乾燥工程で行うことが好ましい。

最後に、乾燥成形体の焼成は、乾燥成形体の大きさにもよるが、通常、 $1410 \sim 1440 \sim 0$ の温度で、 $3 \sim 7$ 時間焼成することが好ましい。また、乾燥工程と焼成工程を連続して行ってもよい。

以下、本発明を実施例により具体的に説明するが、本発明はこれら実施例に限 定されるものではない。

1. 評価方法

後述する実施例及び比較例で得られたハニカムフィルターについて以下に示す 方法で評価を行った。

(1)細孔分布、細孔の平均孔径

マイクロメリティックス社製の水銀圧入式ポロシメーターで細孔分布、平均孔 径を測定した。

(2) 気孔率

コーディエライトの真比重を2.52g/ccとし、全細孔容積から、気孔率

を計算した。

(3) 捕集効率

スートジェネレーターにより煤を発生させた排ガスを、各実施例及び比較例で得られたハニカムフィルターに、一定時間(2分)通過させ、フィルター通過後排ガスに含まれる煤を濾紙で捕集し、煤の重量(W¹)を測定した。また、同じ時間、煤を発生させた排ガスを、フィルターを通過させずに濾紙で捕集し、煤の重量(W²)を測定した。次いで、得られた各重量(W¹)(W²)を以下に示す式(1)に代入して捕集効率を求めた。

 $(W^2 - W^1) / (W^2) \times 100 \cdots (1)$

(4) スート捕集圧損

まず、各実施例及び比較例で得られたハニカムフィルターの両端面に、内径 Φ 130mmのリングを圧接し、このリングを介して、スートジェネレーターで発生させたスートを、ハニカムフィルターの Φ 130mmの範囲内に流入し、10gのスートを捕集させた。

次いで、ハニカムフィルターがスートを捕集した状態で、2.27Nm3/m inの空気を流し、フィルター前後の圧力差を測定して、スートを捕集した状態での圧力損失を評価した。

2. 実施例、及び比較例

実施例1

表1に示す平均粒径及び粒径分布のタルク(平均粒径: 20μ m、粒径 75μ m以上の粉末:4質量%)、溶融シリカB(平均粒径: 35μ m、粒径 75μ m以上の粉末:0.5質量%)、水酸化アルミニウム(平均粒径: 2μ m、粒径 75μ m以上の粉末:0質量%)を、表2に示すように、タルク37質量%、溶融シリカB19質量%、水酸化アルミニウム44質量%の割合で混合してコーディエライト化原料を調製した。

次いで、表2に示すように、このコーディエライト化原料100重量部に対して、グラファイト20重量部、ポリエチレンテレフタレート7重量部、ポリメタ

クリル酸メチル7重量部、ヒドロキシプロピルメチルセルロース4重量部、ラウリン酸カリ石鹸0.5重量部、水30重量部を投入、混練して可塑性とし、この可塑性の原料を、真空土練機でシリンダー状の坏土を成形し、押出し成形機に投入してハニカム状に成形した。

次いで、得られた成形体を、誘電乾燥の後、熱風乾燥で絶乾し、所定の寸法に 両端面を切断した。

次いで、このハニカム状の乾燥体における貫通孔を、同様の組成のコーディエ ライト化原料からなるスラリーで、貫通孔が開口する両端面で互い違いに目封じ した。

最後に、1420℃、4時間、焼成して、サイズ: ϕ 144mm×L152mm、隔壁厚さ:300 μ m、セル数:300セル/inch²のハニカムフィルターを得た。

実施例2

実施例1において、溶融シリカB(平均粒径: 35μ m、粒径 75μ m以上の粉末:0.5質量%)に代え、石英<math>B(平均粒径: 19μ m、粒径 75μ m以上の粉末:0.3質量%)を混合したこと以外は、実施例<math>1と同様にしてハニカムフィルターを得た。

比較例1

実施例1において、溶融シリカB(平均粒径: 35μ m、粒径 75μ m以上の粉末: $0.5質量%)に代え、溶融シリカA(平均粒径:<math>40\mu$ m、粒径 75μ m以上の粉末:6質量%)を混合したこと以外は、実施例1と同様にしてハニカムフィルターを得た。

実施例3

実施例1において、表1に示す平均粒径及び粒径分布のタルク(平均粒径:20 μ m、粒径75 μ m以上の粉末:4質量%)、カオリン(平均粒径:10 μ m、粒径75 μ m以上の粉末:2質量%)、石英D(平均粒径:5 μ m、粒径75 μ m以上の粉末:0.1質量%)、酸化アルミニウム(平均粒径:6 μ m、粒径75 μ m以上の粉末:0.2質量%)水酸化アルミニウム(平均粒径:2 μ m、

粒径 7 5 μm以上の粉末: 0質量%)を、表 2 に示すようにタルク 4 0 質量%、カオリン1質量%、石英D 2 1 質量%、酸化アルミニウム1 9 質量%、水酸化アルミニウム1 9 質量%の割合で混合してコーディエライト化原料を調製したこと、並びに得られたコーディエライト化原料1 0 0 重量部に対して、造孔剤として、グラファイト2 0 重量部、ポリエチレンテレフタレート1 0 重量部、ポリメタクリル酸メチル1 0 重量部を添加したこと以外は、実施例1と同様にしてハニカムフィルターを得た。

実施例4

実施例1において、表1に示す平均粒径及び粒径分布のタルク(平均粒径:20 μ m、粒径75 μ m以上の粉末:4質量%)、カオリン(平均粒径:10 μ m、粒径75 μ m以上の粉末:2質量%)、石英B(平均粒径:19 μ m、粒径75 μ m以上の粉末:0.3質量%)、酸化アルミニウム(平均粒径:6 μ m、粒径75 μ m以上の粉末:0.2質量%)水酸化アルミニウム(平均粒径:2 μ m、粒径75 μ m以上の粉末:0.2質量%)を、表2に示すようにタルク40質量%、カオリン3質量%、石英B20質量%、酸化アルミニウム18質量%、水酸化アルミニウム19質量%の割合で混合してコーディエライト化原料を調製したこと、並びに得られたコーディエライト化原料100重量部に対して、造孔剤として、グラファイト20重量部、ポリエチレンテレフタレート9重量部、ポリメタクリル酸メチル9重量部を添加したこと以外は、実施例1と同様にしてハニカムフィルターを得た。

実施例 5

実施例4において、表2に示すように、表1に示す石英B(平均粒径: 19μ m、粒径 75μ m以上の粉末: $0.3質量%)に代え、石英D(平均粒径: <math>5\mu$ m、粒径 75μ m以上の粉末: 0.1質量%)を混合したこと、並びに得られたコーディエライト化原料 <math>100重量部に対して、造孔剤として、グラファイト 25重量部、ポリエチレンテレフタレート 5重量部、ポリメタクリル酸メチル 10重量部を添加したこと以外は、実施例 4と同様にしてハニカムフィルターを得た

実施例6

実施例4において、表2に示すように、表1に示す石英B(平均粒径:19 μ m、粒径75 μ m以上の粉末:0.3質量%)に代え、石英E(平均粒径:10 μ m、粒径75 μ m以上の粉末:0.1質量%)を混合したこと、並びに得られたコーディエライト化原料100重量部に対して、造孔剤として、グラファイト20重量部、ポリエチレンテレフタレート4重量部を添加したこと以外は、実施例4と同様にしてハニカムフィルターを得た。

実施例7

実施例4において、表2に示すように、表1に示す石英B(平均粒径:19 μ m、粒径75 μ m以上の粉末:0.3質量%)に代え、溶融シリカB(平均粒径:35 μ m、粒径75 μ m以上の粉末:0.5質量%)を混合したこと、並びに得られたコーディエライト化原料100重量部に対して、造孔剤として、グラファイト20重量部、ポリエチレンテレフタレート3重量部、ポリメタクリル酸メチル9重量部を添加したこと以外は、実施例4と同様にしてハニカムフィルターを得た。

実施例8

実施例4において、表2に示すように、表1に示す石英B(平均粒径:19 μ m、粒径75 μ m以上の粉末:0.3質量%)に代え、溶融シリカC(平均粒径:16 μ m、粒径75 μ m以上の粉末:1質量%)を混合したこと、並びに得られたコーディエライト化原料100重量部に対して、造孔剤として、グラファイト10重量部、ポリメタクリル酸メチル17重量部を添加したこと以外は、実施例4と同様にしてハニカムフィルターを得た。

比較例2

実施例4において、表2に示すように、表1に示す石英B(平均粒径:19 μ m、粒径75 μ m以上の粉末:0.3質量%)に代え、石英A(平均粒径:20 μ m、粒径75 μ m以上の粉末:8質量%)を混合したこと、並びに得られたコーディエライト化原料100重量部に対して、造孔剤として、グラファイト20重量部、ポリエチレンテレフタレート7重量部、ポリメタクリル酸メチル9重量

部を添加したこと以外は、実施例4と同様にしてハニカムフィルターを得た。 比較例3

実施例4において、表2に示すように、表1に示す石英B(平均粒径: 19μ m、粒径 75μ m以上の粉末: 0.3質量%)に代え、石英C(平均粒径: 5μ m、粒径 75μ m以上の粉末: 3質量%)を混合したこと、並びに得られたコーディエライト化原料100重量部に対して、造孔剤として、グラファイト20重量部、ポリエチレンテレフタレート10重量部、ポリメタクリル酸メチル10重量部を添加したこと以外は、実施例4と同様にしてハニカムフィルターを得た。比較例4

実施例4において、表2に示すように、表1に示す石英B(平均粒径: 19μ m、粒径 75μ m以上の粉末: $0.3質量%)に代え、溶融シリカD(平均粒径: <math>70\mu$ m、粒径 75μ m以上の粉末: 39質量%)を混合したこと、並びに得られたコーディエライト化原料<math>100重量部に対して、造孔剤として、グラファイト20重量部、ポリエチレンテレフタレート6重量部、ポリメタクリル酸メチル7重量部を添加したこと以外は、実施例4と同様にしてハニカムフィルターを得た。

実施例9

実施例4において、表2に示すように、タルク40質量%、カオリン5質量%、石英B19質量%、酸化アルミニウム17質量%、水酸化アルミニウム19質量%の割合で混合してコーディエライト化原料を調製したこと、並びに得られたコーディエライト化原料100重量部に対して、造孔剤として、グラファイト20重量部、ポリエチレンテレフタレート7重量部、ポリメタクリル酸メチル7重量部を添加したこと以外は、実施例4と同様にしてハニカムフィルターを得た。実施例10

実施例4において、表2に示すように、タルク40質量%、カオリン10質量%、石英B17質量%、酸化アルミニウム16質量%、水酸化アルミニウム17質量%の割合で混合してコーディエライト化原料を調製したこと、並びに得られたコーディエライト化原料100重量部に対して、造孔剤として、グラファイト

10重量部、ポリエチレンテレフタレート8重量部、ポリメタクリル酸メチル15重量部を添加したこと以外は、実施例4と同様にしてハニカムフィルターを得た。

比較例 5

実施例4において、表2に示すように、タルク40質量%、カオリン15質量%、石英B14質量%、酸化アルミニウム15質量%、水酸化アルミニウム16質量%の割合で混合してコーディエライト化原料を調製したこと、並びに得られたコーディエライト化原料100重量部に対して、造孔剤として、グラファイト20重量部、ポリエチレンテレフタレート4重量部、ポリメタクリル酸メチル9重量部を添加したこと以外は、実施例4と同様にしてハニカムフィルターを得た

比較例6

実施例4において、表2に示すように、タルク40質量%、カオリン19質量%、石英B12質量%、酸化アルミニウム14質量%、水酸化アルミニウム15質量%の割合で混合してコーディエライト化原料を調製したこと、並びに得られたコーディエライト化原料100重量部に対して、造孔剤として、グラファイト20重量部、ポリエチレンテレフタレート4重量部、ポリメタクリル酸メチル7重量部を添加したこと以外は、実施例4と同様にしてハニカムフィルターを得た

実施例11

実施例10において、表2に示すように、コーディエライト化原料に、造孔剤として、グラファイト、ポリエチレンテレフタレート、及びポリメタクリル酸メチルを添加せずに、発泡樹脂であるアクリル系マイクロカプセル(商品名:Fー50E、松本油脂製薬株式会社製)を、コーディエライト化原料100重量部に対して2.4重量部投入したこと以外は、実施例10と同様にしてハニカムフィルターを得た。

実施例12

実施例10において、表2に示すように、タルク40質量%、カオリン0質量

%、石英D21質量%、酸化アルミニウム16質量%、水酸化アルミニウム23 質量%の割合で混合してコーディエライト化原料を調製したこと、並びに得られ たコーディエライト化原料100重量部に対して、造孔剤として、グラファイト 10重量部、ポリエチレンテレフタレート5重量部、ポリメタクリル酸メチル5 重量部、及び発泡樹脂であるアクリル系マイクロカプセル1.8重量部を添加し たこと以外は、実施例10と同様にしてハニカムフィルターを得た。

実施例13

実施例10において、表2に示すように、タルク40質量%、カオリン5質量%、石英B19質量%、酸化アルミニウム17質量%、水酸化アルミニウム19質量%の割合で混合してコーディエライト化原料を調製したこと、及び得られたコーディエライト化原料100重量部に対して、造孔剤として、グラファイト20重量部、及び発泡樹脂であるアクリル系マイクロカプセル2.8重量部を添加したこと以外は、実施例10と同様にしてハニカムフィルターを得た。

3. 評価

カオリン及びタルク以外のシリカ源成分が、粒径 75μ m以上の粉末1.0質量%以下の粒径分布を有する実施例 $1\sim13$ では、 50μ mを超える細孔の容積が、全体の細孔容積の10%以下に制御されているハニカムフィルターを得ることができ、このハニカムフィルターでは、85%以上と高い捕集効率を達成することができた。特に、カオリン及びタルク以外のシリカ源成分が、粒径 75μ m以上の粉末を、0.1質量%以下で含有する粒径分布を有する実施例3.5では、 50μ mを超える細孔の容積が、全体の細孔容積の2%以下に制御されているハニカムフィルターを得ることができ、このハニカムフィルターでは、94%以上と極めて高い捕集効率を達成することができた。

一方、カオリン及びタルク以外のシリカ源成分の粒径分布が、粒径75μm以上の粉末を、1.0質量%超過で含有する比較例1~4では、50μmを超える細孔の容積が、全体の細孔容積の10%を超えるハニカムフィルターが得られ、このハニカムフィルターでは、75%以下の低い捕集効率となってしまった。

また、カオリンの含有率が、10質量%以下である実施例1~13では、10

μm未満の細孔容積が、全体の細孔容積の15%以下に制御されているハニカムフィルターを得ることができた。このフィルターに触媒を付けた場合、触媒による細孔の目詰まりが抑制され、煤捕集時の圧力損失が小さいものと推定される。

一方、カオリンの含有率が、10質量%を超える比較例5、6では、10 μ m 未満の細孔容積が、全体の細孔容積の15%を超えるハニカムフィルターが得られた。このハニカムフィルターでは、触媒を付けた場合、触媒による細孔の目詰まりにより圧力損失が大きいものと推定される。

また、コーディエライト化原料100重量部に対して、発泡剤を1.8~2.8重量部添加した実施例11~13では、気孔率が68~75%であるハニカムフィルターを得ることができ、このハニカムフィルターでは、91%以上と高い捕集効率を達成することができ、しかも、捕集圧損が、8.5 (KPa)以下とスート捕集状態での圧力損失が小さかった。

なお、実施例12において、発泡樹脂の添加量を3.2重量部に変更してハニカムフィルターを製造したところ、気孔率80%のハニカムフィルターが得られたものの、構造強度の点で、必ずしも充分なものではなかった。

表1. 原料

| ローディライト化原料成分 | | 粒径75μm以上の |
|--------------|------------|------------|
| | (μ m) | 粉末含有率(質量%) |
| タルク | 20 | 4 . |
| カオリン | 10 | 2 |
| 石英A | 20 | 8 |
| 石英B | 19 | 0.3 |
| 石英C | 5 | 3 |
| 石英D | 5 | 0.1 |
| 石英E | 10 | 0.1 |
| 溶融シリカA | 40 | 6 |
| 溶融シリカB | 35 | 0.5 |
| 溶融シリカC | 16 | 1 |
| 溶融シリカD | 70 | 39 |
| 酸化アルミニウム | 6 | 0.2 |
| 水酸化アルミニウム | 2 | 0 |

| 表2. 原料 | 表2. 原料關合組成(wt%) | | 作団ルンプ | | | | | 造孔剤 | | |
|-------------|-----------------|-----------|------------------|-----------------|------------|--------------------------|---------|--------|--------|---------|
| | | コーナイユ | 4 | 1/4 | エキノンションームノ | また ルンバニーカー コン 部外 ルフルニーウル | カプラファイト | PFT *1 | PMM *2 | 発泡樹脂 #3 |
| So | タラク | セインソークを持つ | いい。 | 温成分 今五数(暦量%) | (短間の) | 小段 [27] (27) (個量%) | (庫魯期) | mini | (重量部) | (重量部) |
| | (真重%) | (貝里70/ | 12.7 | Κ, | | · · | 20 | 7 | 7 | 0 |
| 実施例1 | 37 | 0 | 溶融シルB | 19 | | #: | 2 | | - | C |
| 田佐位り | 37 | 0 | 石英B | 19 | 0 | 44 | 707 | ١ | Ş | |
| 田梅酒の | 40 | - | 石英D | 21 | 19 | 19 | 7.0 | 2 | 2, | |
| 米を記する | | | 上 田 田 田 | 20 | 18 | 19 | 20 | 6 | 6 | |
| 英加加4 | Q. | 2 | | 200 | 18 | 19 | 25 | 5 | 10 | 0 |
| 実施例5 | 40 | 2 | 1747 | 3 6 | 200 | 19 | 20 | 4 | 0 | 0 |
| 実施例6 | 40 | 2) | 177 | 02 | 200 | 10 | 20 | 8 | 6 | 0 |
| 実施例7 | 40 | 2 | を記 | | 0 9 | | 2 | 0 | 11 | 0 |
| 軍怖例8 | 40 | က | 溶融シリカC | | 8 | P (| 2 8 | 3 | - | |
| 田佐何日 | 40 | 5 | 石英B | 19 | 17 | 19 | 0.7 | , | 1 | |
| 中権を行う | | 10 | 七 描 B | 17 | 16 | 17 | 9 | 8 | 61 | |
| 本語のこと | | 2 | 一加御一 | 17 | 91 | 17 | 0 | 0 | 0 | 2.4 |
| 米馬河二 | | 2 0 | NHW) | 21 | 16 | 23 | 10 | 2 | 5 | 1.8 |
| 来临河 12 | 40 | 2 | が開出 | 10 | 11 | 19 | 22 | 0 | 0 | 2.8 |
| 米高がこ | | | | | C | 44 | 20 | 7 | 7 | 0 |
| 元数 2 | 3/ | | /中間///// | | 18 | 10 | 20 | 7 | 6 | 0 |
| 比較例2 | 40 | 20 | 白茶の | 07 | 9 | 0 | S | 9 | 10 | 0 |
| 比較例3 | 49 | 20 | 14条0 | | 0 0 | 2 2 | 20 | œ | 1 | 0 |
| 比較例4 | 40 | 3 | が配がかり | | 0 1 | 97 | 2 6 | | a | 0 |
| 比較例5 | 40 | 15 | 石英B | 14 | 62 | 0 2 | 25 | | , | 0 |
| 比較例6 | 40 | 19 | 石英B | 12 | 14 | cı cı | 20 | - | | |

* 1 FEI:ホッエアンハップ・ * 2 PMM:ポッメタッリル酸メチル * 3 発泡樹脂:アツリル系マイクロカブセル

捕集劾率 (%) 88 89 93 89 89 89 89 89 2 88 68 75 48 91 捕集圧損 (KPa) 9.4 8.9 8.7 9.0 8.5 10.4 9.6 10.2 8.5 7.8 9.7 9.1 9.4 10.1 9.1 8.7 熱膨張係数 (×10-⁶/°C) 平均細孔径 (m n) 28 17 21 $50 \, \mu \, \text{m}$ 9 9500 38 6 ကြထ $\sim 10 \, \mu \, \text{m}$ က 8 5 5 5 9 225 8 2 4 5 気孔率 (%) 65 65 無極例1 無極例2 無極例3 無極例4 無極例6 無極例6 無極例6 無極例7 無極例9 無極例10 無極例10 無極例11 無極例11 比較例3 比較例3 比較例4 比較例6 ė Ž

表3. 特性

産業上の利用可能性

以上説明したように、本発明の多孔質ハニカムフィルター及びその製造方法によれば、パテキュレート等の捕集効率が高く、かつ細孔の目詰まりによる圧力損失の増大を防止することができ、特に、近年の高圧燃料噴射、コモンレール等を採用したディーゼルエンジンに対応してこれらの特性を発揮することができる多れ質ハニカムフィルター及びその製造方法を提供することができる。

請求の範囲

1. 細孔分布を制御したコーディライトを主結晶相とする材料からなる多孔質 ハニカムフィルターであって、

前記細孔分布が、細孔径 10μ m未満の細孔容積:全細孔容積の15%以下、細孔径 $10\sim50\mu$ mの細孔容積:全細孔容積の75%以上、細孔径 50μ mを超える細孔容積:全細孔容積の10%以下、であることを特徴とする多孔質ハニカムフィルター。

- 2. ハニカムフィルターの気孔率が、 $50 \sim 75\%$ である請求項1に記載の多れ質ハニカムフィルター。
- 3. ハニカムフィルターの気孔率が、65~75%である請求項2に記載の多 孔質ハニカムフィルター。
- 4. ハニカムフィルターの40~800℃における熱膨張係数が、1.0×10-6/℃以下である請求項1~3のいずれか一項に記載の多孔質ハニカムフィルター。
- 5. コーディエライト化原料を主原料とするセラミックス原料を用いる多孔質 ハニカムフィルターの製造方法であって、

前記コーディエライト化原料が、カオリンを、 $0\sim10$ 質量%以下で含有し、かつカオリン及びタルク以外のシリカ(SiO_2)源成分を、粒径 75μ m以上の粉末が1質量%以下で含有する粒径分布としたことを特徴とする多孔質ハニカムフィルターの製造方法。

- 6. 前記コーディエライト化原料が、前記カオリンを、1~10質量%で含有する請求項5に記載の多孔質ハニカムフィルターの製造方法。
- 7. 前記カオリン及び前記タルク以外のシリカ(SiO,)源成分が、石英、 又は溶融シリカの少なくとも一種を含有するものである請求項5又は6に記載の 多孔質ハニカムフィルターの製造方法。
- 8. 前記コーディエライト化原料が、アルミナ(A1₂O₃)源成分として、酸化アルミニウム、又は水酸化アルミニウムの少なくとも一種を含有する請求項5

- ~7のいずれか一項に記載の多孔質ハニカムフィルターの製造方法。
- 9. 前記アルミナ $(A1_2O_3)$ 源成分として、粒径 $1\sim10~\mu$ mの水酸化アルミニウムを $15\sim45$ 質量%含有する請求項8に記載の多孔質ハニカムフィルターの製造方法。
- 10. 前記アルミナ (Al_2O_3) 源成分として、粒径 $4\sim8~\mu$ mの酸化アルミニウムを $0\sim2$ 0 質量%含有する請求項 8 又は 9 に記載の多孔質ハニカムフィルターの製造方法。
- 11. 前記コーディエライト化原料が、マグネシア (MgO) 源成分として、 タルクを37~40質量%含有する請求項5~10のいずれか一項に記載の多孔 質ハニカムフィルターの製造方法。
- 12. 前記タルクの粒径が、 $5\sim40~\mu\,\mathrm{m}$ である請求項11に記載の多孔質ハニカムフィルターの製造方法。
- 13. 該セラミックス原料が、該コーディエライト化原料 100 重量部に対して、発泡樹脂を $1\sim4$ 重量部含有する請求項 $5\sim12$ のいずれか一項に記載の多れ質ハニカムフィルターの製造方法。

INTERNATIONAL SEARCH REPORT

International application No.

PCT/JP01/08720

| | | | 101/0 | F01/00/20 |
|----------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------|-------------------------------------------------------------------------------------------------------------------------|----------------------------|---------------------------------------------------|----------------------------------|
| | SIFICATION OF SUBJECT MATTER .C1 ⁷ B01D39/20, F01N3/02, B01D4 | 1 6/00 | | |
| According to | o International Patent Classification (IPC) or to both na | ational classification ar | nd IPC | |
| | S SEARCHED | | | |
| Int. | ocumentation searched (classification system followed . Cl ⁷ B01D39/20, F01N3/02, B01D4 | 46/00 | · | |
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発明の属する分野の分類(国際特許分類(IPC))

Int. Cl' B01D39/20, F01N3/02, B01D46/00

B. 調査を行った分野

調査を行った最小限資料(国際特許分類(IPC))

Int. C1' B01D39/20, F01N3/02, B01D46/00

最小限資料以外の資料で調査を行った分野に含まれるもの

日本国実用新案公報

1926-1996年

日本国公開実用新案公報

1971-2001年

日本国登録实用新案公報

1994-2001年

日本国実用新案登録公報

1996-2001年

国際調査で使用した電子データベース(データベースの名称、調査に使用した用語)

WPI (DIALOG)

| C. 関連する | 5と認められる文献 | · |
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区欄の続きにも文献が列挙されている。

□ パテントファミリーに関する別紙を参照。

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